

'MODELLING FOR GEOCHEMISTS' EVERYTHING YOU ALWAYS WANTED TO KNOW ABOUT MODELLING, BUT WERE AFRAID TO ASK!

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INTRODUCTION

During previous SWIM's, we noted some of the modellers lacked the knowledge to fully appreciate the papers of the chemists and the other way round. To make the papers of the other 'root' of our work better understandable, the 17th SWIM included two parallel lectures. In this one, the practise of modelling will be explained to those usually concerned with chemistry. The other course explains the basics of hydrogeochemical studies to the modellers.

This is not a 'regular' paper. Instead of writing text, I preferred to hand in my presentation sheets as a paper. This paper should give a refreshing view on the subject. In my opinion, this time sheets are better than words. No bullshit and to the (power)point !! I hope anyone who reads this, will know the ins and outs of groundwater modelling.

Modelling for Chemists

*Everything you always wanted to know about
modelling, but were afraid to ask!*

- Modelling protocol
- Discretisation Partial Differential Equation (PDE)
- Groundwater flow: MODFLOW
- Solute transport: MOC3D

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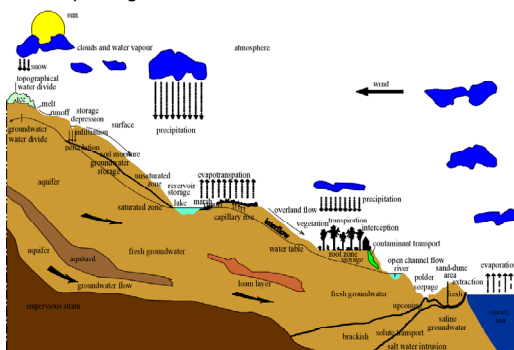
SWIM17: 6-10 May 2002

Modelling for Chemists

- Difficult to determine target group for this lecture
- No density differences considered
- I like equations, so don't be shocked by the PDEs
- 45 min.: not enough to understand it all completely
- These sheets will be available

SWIM17: 6-10 May 2002

The Hydrological Cycle



Ten steps of the Modelling Protocol

1. Problem definition
2. Purpose definition
3. Conceptualisation
4. Selection computer code
5. Model design
6. Calibration
7. Verification
8. Simulation
9. Presentation
10. Postaudit

MODELLING PROTOCOL

IMPORTANT

Modelling protocol

Why numerical modelling?

- +:
- cheaper than scale models
- analysis of very complex systems is possible
- a model can be used as a database
- :
- simplification of the reality
- only a tool, no purpose on itself
- garbage in=garbage out: (field)data important
- perfect fit measurement and simulation is suspicious

IMPORTANT

Modelling protocol

3. Conceptualisation (I)

Model is only a schematisation of the reality

Which hydro(geo)logical processes are relevant?

Which processes can be neglected?

Boundary conditions

Variables and parameters:

- subsoil parameters
- fluxes in and out
- initial conditions
- geochemical data

Mathematical equations

Modelling protocol

3. Concept (II): example of salt water intrusion

Relevant processes:

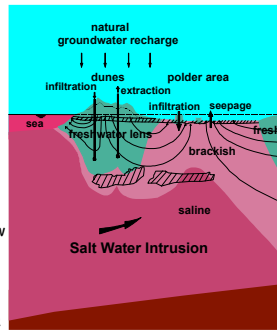
- groundwater flow in a heterogeneous porous medium
- solute transport
- variable density flow
- natural recharge
- extraction of groundwater

Negligible processes:

- heat flow
- swelling of clayey aquitard
- non-steady groundwater flow

Boundary conditions

- no flow at bottom
- flux in dune area
- constant head in polder area



4. Selection computer code

There are numerous good groundwater computer codes!

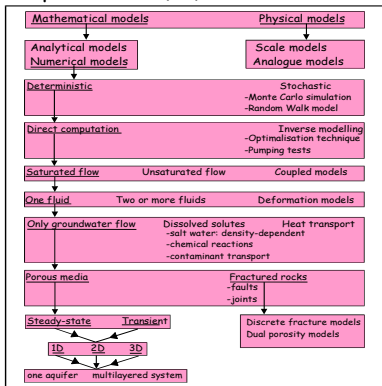
See internet, e.g.:

USGS: water.usgs.gov/nrp/gwsoftware/
 Scientific Software Group: www.scisoftware.com/

4. Selection computer code (II)

water.usgs.gov/nrp/gwsoftware/
www.scisoftware.com/

Groundwater computer codes



Modelling protocol

5. Model design (I)

Choice grid Δx :

- depends on natural variation in the groundwater system
- concept model
- data collection

Choice time step Δt

Conditions:

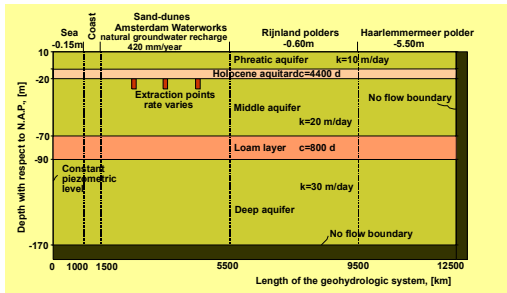
- initial conditions
- boundary conditions:
 1. Dirichlet: head
 2. Neumann: flux, e.g., no flow
 3. Cauchy: mixed boundary condition

Modelling protocol **IMPORTANT**

Modelling protocol

5. Model design (II): example

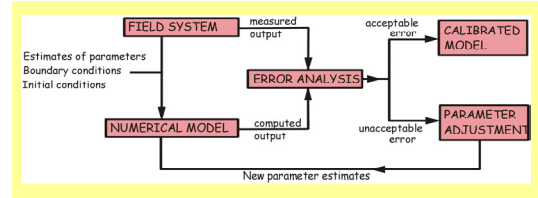
Geometry, subsoil parameters, boundary conditions



6. Calibration (I)

Fitting the groundwater model: is your model okay?

- trial and error
- automatic parameter estimation/inverse modelling (PEST, UCODE)

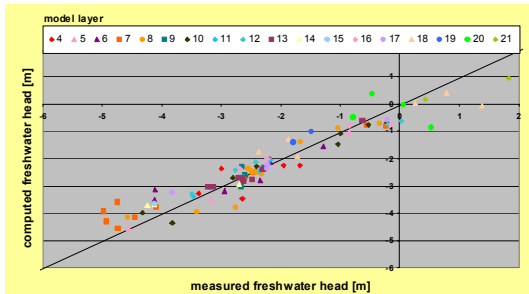


Modelling protocol **IMPORTANT**

Modelling protocol

6. Calibration (II): example

Measured and computed freshwater heads



6. Calibration: errors during modelling protocol

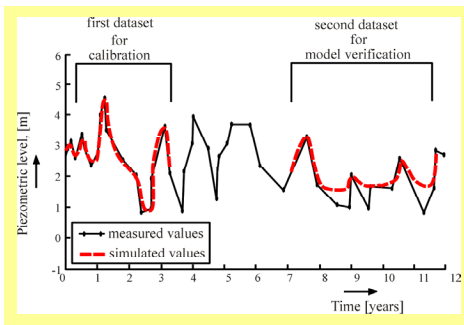
- Wrong model concept
- Incomplete equations
- Inaccurate parameters and variables
- Errors in computer code
- Numerical inaccuracies

IMPORTANT

Modelling protocol

Modelling protocol

7. Verification: testing the calibrated model



'verification problem': there is always a lack of data

8. Simulation

Simulation of scenarios

Computation time depends on:

- computer speed
- size model
- efficiency compiler
- output format

9. Presentation

10. Postaudit

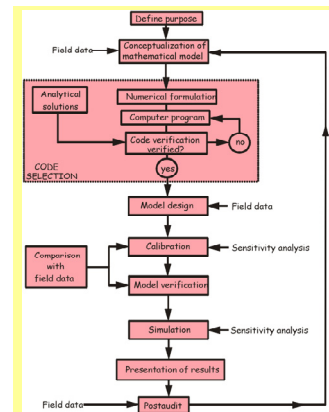
Postaudit: analysing model results after a long time

Anderson & Woessner('92): four postaudits from the 1960's

Errors in model results are mainly caused by:

- wrong concept
- wrong scenarios

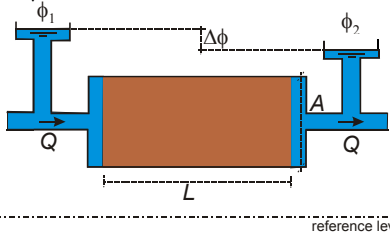
Modelling scheme



Modelling protocol

DISCRETIZATION PDE

I. Darcy's law (1856)



$$Q \propto \phi_1 - \phi_2 \quad Q \propto \frac{1}{L} \quad Q \propto A \quad \text{gives} \quad Q \propto A \frac{\phi_1 - \phi_2}{L}$$

$$Q = KA \frac{\phi_1 - \phi_2}{L} \quad \text{where } K = \text{hydraulic conductivity [L/T]}$$

Discretisation PDE

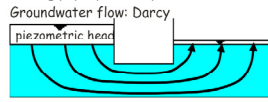
II. Darcy's Law

$$q_x = -k_x \frac{\partial \phi}{\partial x} \quad q_y = -k_y \frac{\partial \phi}{\partial y} \quad q_z = -k_z \frac{\partial \phi}{\partial z}$$

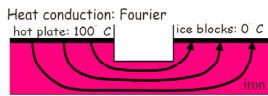
q =Darcian specific discharge [L/T]
 ϕ =piezometric head [L]
 k =hydraulic conductivity [L/T]

Discretisation PDE

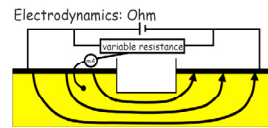
Analogy physical processes



$$q = -k \frac{\partial \phi}{\partial x}$$



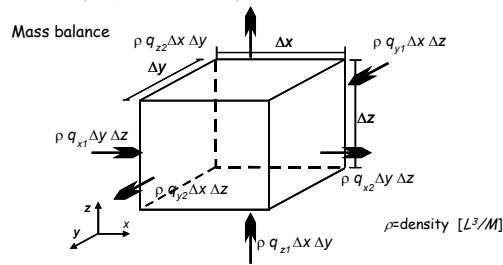
$$h = -\lambda \frac{\partial T}{\partial x}$$



$$i = -\sigma \frac{\partial V}{\partial x}$$

Discretisation PDE

Continuity equation: steady state



$$\frac{\partial \rho q_x}{\partial x} + \frac{\partial \rho q_y}{\partial y} + \frac{\partial \rho q_z}{\partial z} = 0$$

Discretisation PDE

IMPORTANT

Steady state groundwater flow equation (PDE=Partial Differential Equation)

Flow equation (Darcy's Law) $q_x = -k_x \frac{\partial \phi}{\partial x} \quad q_y = -k_y \frac{\partial \phi}{\partial y} \quad q_z = -k_z \frac{\partial \phi}{\partial z}$

+ Continuity equation $\frac{\partial \rho q_x}{\partial x} + \frac{\partial \rho q_y}{\partial y} + \frac{\partial \rho q_z}{\partial z} = 0$

Groundwater flow equation

$$\frac{\partial}{\partial x} \left(-k_x \frac{\partial \phi}{\partial x} \right) + \frac{\partial}{\partial y} \left(-k_y \frac{\partial \phi}{\partial y} \right) + \frac{\partial}{\partial z} \left(-k_z \frac{\partial \phi}{\partial z} \right) = 0$$

If k =constant and ρ =constant then:

$$\frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} + \frac{\partial^2 \phi}{\partial z^2} = 0 \quad \text{Laplace equation}$$

$$\nabla^2 \phi = 0$$

Discretisation PDE

IMPORTANT

Taylor series development (I)

Best estimate of ϕ_{i+1} is based on ϕ_i

$$\phi_{i+1} = \phi_i + \Delta x \frac{\partial \phi_i}{\partial x} + \frac{1}{2} \Delta x^2 \frac{\partial^2 \phi_i}{\partial x^2} + \frac{1}{6} \Delta x^3 \frac{\partial^3 \phi_i}{\partial x^3} + \frac{1}{24} \Delta x^4 \frac{\partial^4 \phi_i}{\partial x^4} + K$$

$$\phi_{i-1} = \phi_i - \Delta x \frac{\partial \phi_i}{\partial x} + \frac{1}{2} \Delta x^2 \frac{\partial^2 \phi_i}{\partial x^2} - \frac{1}{6} \Delta x^3 \frac{\partial^3 \phi_i}{\partial x^3} + \frac{1}{24} \Delta x^4 \frac{\partial^4 \phi_i}{\partial x^4} + K$$

$$\phi_{i+1} - \phi_{i-1} = 2\Delta x \frac{\partial \phi_i}{\partial x} + \frac{1}{3} \Delta x^3 \frac{\partial^3 \phi_i}{\partial x^3} + K$$

$$\frac{\partial \phi_i}{\partial x} = \frac{\phi_{i+1} - \phi_{i-1}}{2\Delta x} + O\left(-\frac{1}{6} \Delta x^2 \frac{\partial^3 \phi_i}{\partial x^3} + K\right)$$

Discretisation PDE

IMPORTANT

Discretisation PDE

Taylor series development (II)

$$\begin{aligned} \phi_{i+1} &= \phi_i + \Delta x \frac{\partial \phi_i}{\partial x} + \frac{1}{2} \Delta x^2 \frac{\partial^2 \phi_i}{\partial x^2} + \frac{1}{6} \Delta x^3 \frac{\partial^3 \phi_i}{\partial x^3} + \frac{1}{24} \Delta x^4 \frac{\partial^4 \phi_i}{\partial x^4} + K \\ \phi_{i-1} &= \phi_i - \Delta x \frac{\partial \phi_i}{\partial x} + \frac{1}{2} \Delta x^2 \frac{\partial^2 \phi_i}{\partial x^2} - \frac{1}{6} \Delta x^3 \frac{\partial^3 \phi_i}{\partial x^3} + \frac{1}{24} \Delta x^4 \frac{\partial^4 \phi_i}{\partial x^4} + K \end{aligned}$$

$$\phi_{i+1} + \phi_{i-1} = 2\phi_i + \Delta x^2 \frac{\partial^2 \phi_i}{\partial x^2} + \frac{1}{12} \Delta x^4 \frac{\partial^4 \phi_i}{\partial x^4} + K$$

$$\frac{\partial^2 \phi_i}{\partial x^2} = \frac{\phi_{i+1} - 2\phi_i + \phi_{i-1}}{\Delta x^2} + O\left(-\frac{1}{12} \Delta x^2 \frac{\partial^4 \phi_i}{\partial x^4} + K\right)$$

IMPORTANT

Discretisation PDE

Laplace equation in 2D

$$\nabla^2 \phi = 0 \Leftrightarrow \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} = 0$$

Discretisation in x-direction (i): $\frac{\partial^2 \phi_{i,j}}{\partial x^2} = \frac{\phi_{i+1,j} - 2\phi_{i,j} + \phi_{i-1,j}}{\Delta x^2}$

Discretisation in y-direction (j): $\frac{\partial^2 \phi_{i,j}}{\partial y^2} = \frac{\phi_{i,j+1} - 2\phi_{i,j} + \phi_{i,j-1}}{\Delta y^2}$

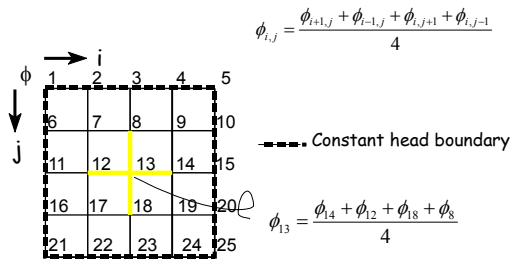
$$\frac{\phi_{i+1,j} - 2\phi_{i,j} + \phi_{i-1,j}}{\Delta x^2} + \frac{\phi_{i,j+1} - 2\phi_{i,j} + \phi_{i,j-1}}{\Delta y^2} = 0$$

If $\Delta x = \Delta y$ then: $\phi_{i+1,j} + \phi_{i-1,j} - 4\phi_{i,j} + \phi_{i,j+1} + \phi_{i,j-1} = 0$

$$\phi_{i,j} = \frac{\phi_{i+1,j} + \phi_{i-1,j} + \phi_{i,j+1} + \phi_{i,j-1}}{4} \quad \text{'Fivepoint operator'}$$

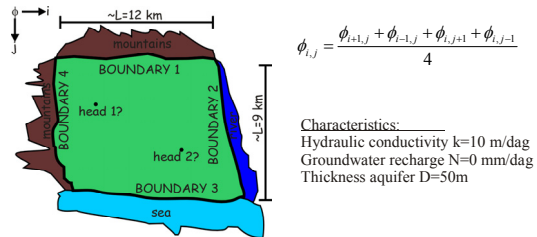
Discretisation PDE

Fivepoint operator: constant head example (I)



Discretisation PDE

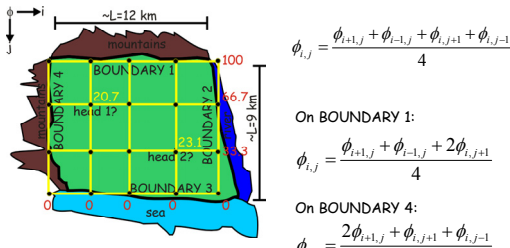
Fivepoint operator: example (II)



Boundary conditions
 BOUNDARY 1: no-flow near the mountains
 BOUNDARY 2: linear from 100 m (near mountains) to 0 m (near sea)
 BOUNDARY 3: constant seawater level of 0 m
 BOUNDARY 4: no-flow

Discretisation PDE

Fivepoint operator: example (III)

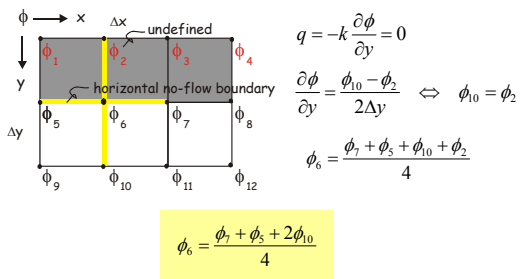


- Initial estimate head=50m
- Convergence-criterion=0.01m
- Number of iterations=74

Discretisation PDE

Fivepoint operator: No-flow example (I)

Nodes on the edges of an element



Discretisation PDE

Non steady state groundwater flow equation

Flow equation (Darcy's Law) $q_x = -k \frac{\partial \phi}{\partial x}$ $q_y = -k \frac{\partial \phi}{\partial y}$ $q_z = -k \frac{\partial \phi}{\partial z}$

Non steady state continuity equation $\frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z} = S_s \frac{\partial \phi}{\partial t} + W'$

Groundwater flow equation S_s =specific storage coefficient [L/L] W' =source-term

$$\frac{\partial}{\partial x} \left(-k \frac{\partial \phi}{\partial x} \right) + \frac{\partial}{\partial y} \left(-k \frac{\partial \phi}{\partial y} \right) + \frac{\partial}{\partial z} \left(-k \frac{\partial \phi}{\partial z} \right) = S_s \frac{\partial \phi}{\partial t} + W'$$

Multiply with constant thickness D of the aquifer gives:

$$T \frac{\partial^2 \phi}{\partial x^2} + T \frac{\partial^2 \phi}{\partial y^2} + T \frac{\partial^2 \phi}{\partial z^2} = S \frac{\partial \phi}{\partial t} + W \quad S=\text{elastic storage coefficient [-]} \quad T=kD=\text{transmissivity [L}^2/\text{T]}$$

Discretisation PDE

Explicit numerical 1D solution

One-dimensional non steady state groundwater flow equation:

$$S \frac{\partial \phi}{\partial t} = T \frac{\partial^2 \phi}{\partial x^2} + N$$

Explicit ('forwards in space'):

$$\frac{\partial^2 \phi_i}{\partial x^2} \approx \frac{\phi_{i+1}^i - 2\phi_i^i + \phi_{i-1}^i}{\Delta x^2} \quad \frac{\partial \phi_i}{\partial t} \approx \frac{\phi_i^{i+M} - \phi_i^i}{\Delta t}$$

$$\phi_i^{i+M} = \phi_i^i + \frac{N\Delta t}{S} + \frac{T\Delta t}{S\Delta x^2} (\phi_{i+1}^i - 2\phi_i^i + \phi_{i-1}^i)$$

Properties:

- Direct solution
- Can be numerical instable

MODFLOW

IMPORTANT

MODFLOW

MODFLOW

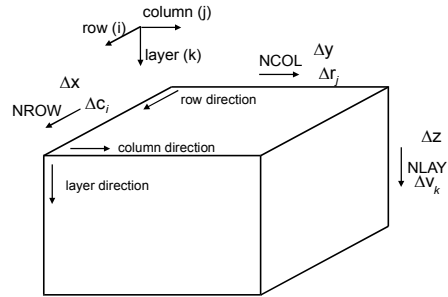
MODFLOW

a modular 3D finite-difference ground-water flow model

(M.G. McDonald & A.W. Harbaugh, from 1983 on)

- USGS, 'public domain'
- non steady state
- heterogeneous porous medium
- anisotropy
- coupled to reactive solute transport
MOC3 (Konikow *et al*, 1996)
MT3D, MT3DMS (Zheng, 1990)
RT3D
- easy to use due to numerous Graphical User Interfaces (GUI's)
PMWIN, GMS, Visual Modflow, Argus One, Groundwater Vistas, etc.

Nomenclature MODFLOW element



MODFLOW

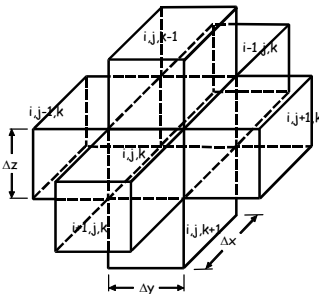
IMPORTANT

MODFLOW

MODFLOW: start with water balance of one element [i,j,k]

Continuity equation (I)

In - Out = Storage



$$\frac{\partial}{\partial x} \left(k_{xx} \frac{\partial \phi}{\partial x} \right) + \frac{\partial}{\partial y} \left(k_{yy} \frac{\partial \phi}{\partial y} \right) + \frac{\partial}{\partial z} \left(k_{zz} \frac{\partial \phi}{\partial z} \right) - W = S_s \frac{\partial \phi}{\partial t}$$

$$\sum Q_i = S_s \frac{\Delta \phi}{\Delta t} \Delta V$$

MODFLOW

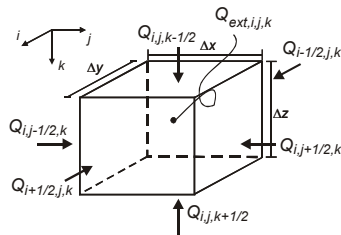
IMPORTANT

MODFLOW

Continuity equation (II)

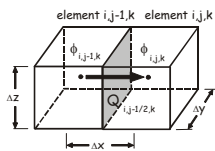
$$\sum Q_i = S_s \frac{\Delta \phi}{\Delta t} \Delta V$$

In = positive



$$Q_{i,j-1/2,k} + Q_{i,j+1/2,k} + Q_{i-1/2,j,k} + Q_{i+1/2,j,k} + Q_{i,j,k-1/2} + Q_{i,j,k+1/2} + Q_{ext,i,j,k} = SS_{i,j,k} \frac{\phi_{i,j,k}^t - \phi_{i,j,k}^{t+\Delta t}}{\Delta t} \Delta V$$

Flow equation (Darcy's Law)



$$Q = \text{surface} * q = \text{surface} * k \frac{\partial \phi}{\partial x}$$

$$Q_{i,j-1/2,k} = k_{i,j-1/2,k} \Delta y \Delta z \frac{\phi_{i,j-1,k} - \phi_{i,j,k}}{\Delta x}$$

$$Q_{i,j-1/2,k} = CR_{i,j-1/2,k} (\phi_{i,j-1,k} - \phi_{i,j,k})$$

where $CR_{i,j-1/2,k} = \frac{k_{i,j-1/2,k} \Delta y \Delta z}{\Delta x}$ is the conductance [L²/T]

MODFLOW

Groundwater flow equation

$$\begin{aligned}
 Q_{i,j-1/2,k} &= CR_{i,j-1/2,k}(\phi_{i,j-1,k} - \phi_{i,j,k}) \\
 Q_{i,j+1/2,k} &= CR_{i,j+1/2,k}(\phi_{i,j+1,k} - \phi_{i,j,k}) \\
 Q_{i-1/2,j,k} &= CC_{i-1/2,j,k}(\phi_{i-1,j,k} - \phi_{i,j,k}) \\
 Q_{i+1/2,j,k} &= CC_{i+1/2,j,k}(\phi_{i+1,j,k} - \phi_{i,j,k}) \\
 Q_{i,j,k-1/2} &= CV_{i,j,k-1/2}(\phi_{i,j,k-1} - \phi_{i,j,k}) \\
 Q_{i,j,k+1/2} &= CV_{i,j,k+1/2}(\phi_{i,j,k+1} - \phi_{i,j,k})
 \end{aligned}$$

$$Q_{i,j-1/2,k} + Q_{i,j+1/2,k} + Q_{i-1/2,j,k} + Q_{i+1/2,j,k} + Q_{i,j,k-1/2} + Q_{i,j,k+1/2} + Q_{ext,i,j,k} = SS_{i,j,k} \frac{\phi_{i,j,k}^t - \phi_{i,j,k}^{t+\Delta t}}{\Delta t} \Delta V$$

MODFLOW

IMPORTANT

The MODFLOW Groundwater flow equation

$$Q_{i,j-1/2,k} + Q_{i,j+1/2,k} + Q_{i-1/2,j,k} + Q_{i+1/2,j,k} + Q_{i,j,k-1/2} + Q_{i,j,k+1/2} + Q_{ext,i,j,k} = SS_{i,j,k} \frac{\phi_{i,j,k}^t - \phi_{i,j,k}^{t+\Delta t}}{\Delta t} \Delta V$$

and:

$$Q_{ext,i,j,k} = P_{i,j,k} \phi_{i,j,k}^{t+\Delta t} + Q'_{i,j,k}$$

gives:

$$\begin{aligned}
 &CV_{i,j,k-1/2} \phi_{i,j,k-1}^{t+\Delta t} + CC_{i-1/2,j,k} \phi_{i-1,j,k}^{t+\Delta t} + CR_{i,j+1/2,k} \phi_{i,j+1,k}^{t+\Delta t} \\
 &+ (-CV_{i,j,k+1/2} - CC_{i+1/2,j,k} - CR_{i,j-1/2,k} - CC_{i-1/2,j,k} - CV_{i,j,k-1/2} + HCOF_{i,j,k}) \phi_{i,j,k}^{t+\Delta t} \\
 &+ CR_{i,j+1/2,k} \phi_{i,j+1,k}^{t+\Delta t} + CC_{i+1/2,j,k} \phi_{i+1,j,k}^{t+\Delta t} + CV_{i,j,k+1/2} \phi_{i,j,k+1}^{t+\Delta t} = RHS_{i,j,k}
 \end{aligned}$$

with:

$$\begin{aligned}
 HCOF_{i,j,k} &= P_{i,j,k} - SC1_{i,j,k} / (\Delta t) \\
 RHS_{i,j,k} &= -Q'_{i,j,k} - SC1_{i,j,k} \phi_{i,j,k}^t / (\Delta t) \\
 SC1_{i,j,k} &= SS_{i,j,k} \Delta V
 \end{aligned}$$

MODFLOW

Boundary conditions in MODFLOW (I)

Example of a system with three types of boundary conditions

Numeric model

0	1	1	1	1	0	0	0	0	0	0	0	1	1	1	1	0	0
1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	0
1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	0
0	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	0
0	0	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	0
0	0	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	0
0	0	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	0
0	0	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	0
0	0	0	0	0	1	1	1	1	1	1	1	1	1	1	1	0	0
0	0	0	0	0	0	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	0	0

MODFLOW

Boundary conditions in MODFLOW (II)

For a constant head condition: IBOUND<0
 For a no flow condition: IBOUND=0
 For a variable head: IBOUND>0

MODFLOW

IMPORTANT

Packages in MODFLOW

1. Well package
2. River package
3. Recharge package
4. Drain package
5. Evaporation package
6. General head package

MODFLOW

1. Well package

$$Q_{well} = Q_{i,j,k}$$

Example: an extraction of 10 m³ per day should be inserted in an element as $Q_{ext,i,j,k} = -10$ (in = positive)

MODFLOW

2. River package (I)

$$Q_{riv} = KLW \left(\frac{\phi_{riv} - \phi_{i,j,k}}{M} \right)$$

$$Q_{riv} = \frac{KLW}{M} (\phi_{riv} - \phi_{i,j,k}) \Leftrightarrow Q_{riv} = C_{riv} (\phi_{riv} - \phi_{i,j,k})$$

MODFLOW

2. River package (II)

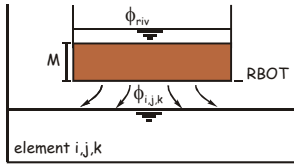
Determine the conductance of the river in one element:

where $C_{riv} = \frac{KLW}{M}$ is the conductance [L²/T] of the river

MODFLOW

2. River package (III)

Leakage to the groundwater system

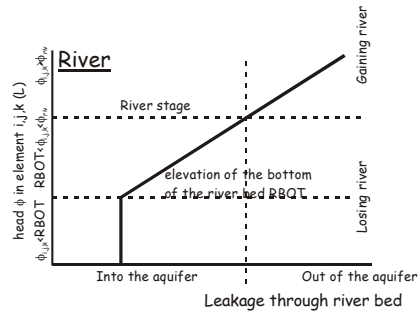


Special case:

if $\phi_{i,j,k} < RBOT$, then $Q_{riv} = C_{riv}(\phi_{riv} - RBOT)$

MODFLOW

2. River package (IV)



MODFLOW

3. Recharge package

$Q_{rec} = I\Delta x\Delta y$

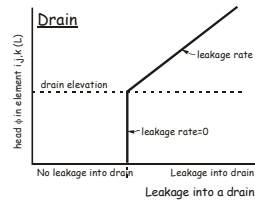
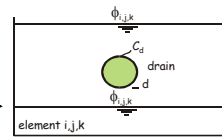
MODFLOW

4. Drain package

$Q_{drm} = C_{drm}(\phi_{i,j,k} - d)$

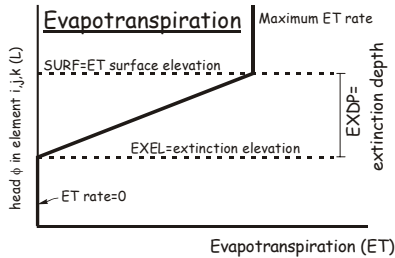
Special case:

if $\phi_{i,j,k} < d$ then $Q_{drm} = 0$



MODFLOW

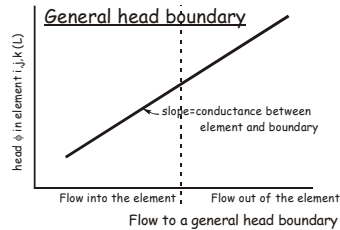
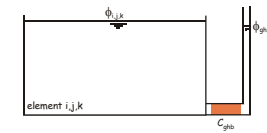
5. Evapotranspiration package



MODFLOW

6. General head boundary package

$Q_{ghb} = C_{ghb}(\phi_{ghb} - \phi_{i,j,k})$



MODFLOW

Time indication MODFLOW

- ITMUNI=1: seconde
- ITMUNI=2: minute
- ITMUNI=3: hour
- ITMUNI=4: day
- ITMUNI=5: year

MOC3D

Solute transport equation

MOC3D

Partial differential equation (PDE):

$$R_d \frac{\partial C}{\partial t} = \frac{\partial}{\partial x_i} \left(D_{ij} \frac{\partial C}{\partial x_j} \right) - \frac{\partial}{\partial x_i} (C V_i) + \frac{(C - C^*)W}{n_e} - R_d \lambda C$$

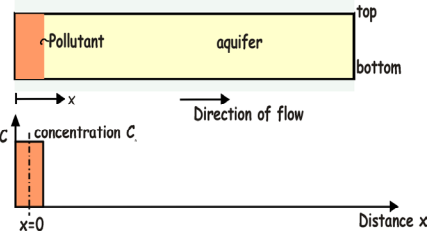
change in concentration dispersion advection source/sink decay

D_{ij} =hydrodynamic dispersion [$L^2 T^{-1}$]
 R_d =retardation factor [-]
 λ =decay-term [T^{-1}]

Solute transport equation: column test (I):

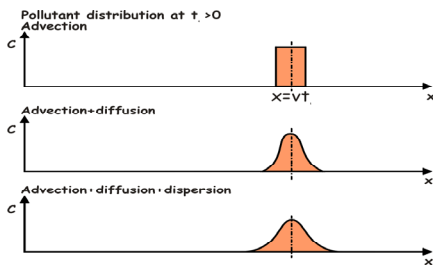
MOC3D

Pollutant distribution at $t=0$



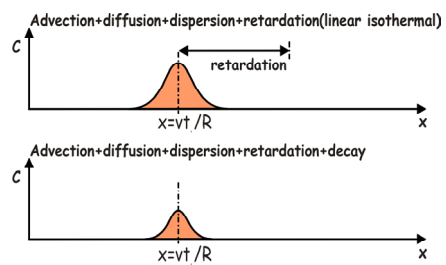
Solute transport equation: column test (II):

MOC3D



Solute transport equation: column test (III):

MOC3D



Hydrodynamic dispersion

MOC3D

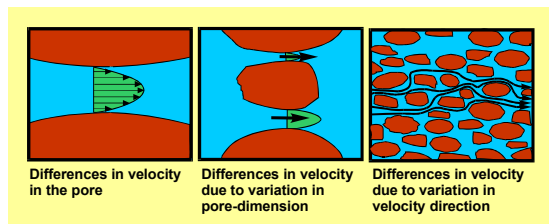
$$\text{hydrodynamic dispersion} = \text{mechanical dispersion} + \text{diffusion}$$

mechanical dispersion:
 tensor
 velocity dependent

diffusion:
 molecular process
 solutes spread due to concentration differences

Mechanical dispersion

MOC3D



IMPORTANT

Method of Characteristics (MOC)

MOC3D

Solve the advection-dispersion equation (ADE) with the Method of Characteristics

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x_i} \left(D_{ij} \frac{\partial C}{\partial x_j} \right) - \frac{\partial}{\partial x_i} (CV_i) + \frac{(C-C)W}{n_e}$$

Lagrangian approach:

Splitting up the advection part and the dispersion/source part:

- advection by means of a particle tracking technique
- dispersion/source by means of the finite difference method

Advantage of the approach of MOC?

MOC3D

It is difficult to solve the whole advection-dispersion equation in one step, because the so-called Peclet-number is high in most groundwater flow/solute transport problems.

(hyperbolic form of the equation is dominant)

The Peclet number stands for the ratio between advection and dispersion

IMPORTANT

Procedure of MOC: advective transport by particle tracking

MOC3D

- Place a number of particles in each element
- Determine the effective velocity of each particle by (b)linear interpolation of the velocity field which is derived from MODFLOW
- Move particles during one solute time step Δt_{solute}
- Average values of all particles in an element to one node value
- Calculate the change in concentration in all nodes due to advective transport
- Add this result to dispersive/source changes of solute transport

Steps in MOC-procedure

MOC3D

1. Determine concentration gradients at old timestep k-1
2. Move particles to model advective transport
3. Concentration of particles to concentration in element node
4. Determine concentration gradients on new timestep k*
5. Determine concentration in element node after advective, dispersive/source transport on timestep k

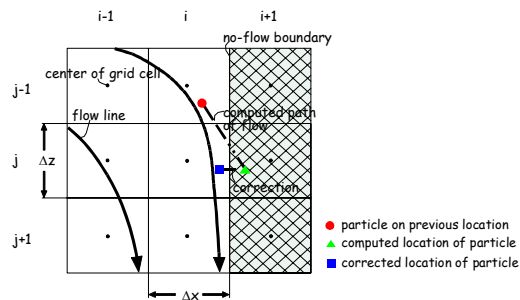
MOC3D

Causes of errors in MOC-procedure

1. Concentration gradients
2. Average from particles to node element, and visa versa
3. Concentration of sources/sinks to entire element
4. Empty elements
5. No-flow boundary: reflection in boundary

Reflection in boundary

MOC3D



MOC3D

Stability criteria (I)

Stability criteria are necessary because the ADE is solved explicitly

1. Neumann criterion:

$$\frac{D_{xx} \Delta t_s}{\Delta x^2} + \frac{D_{yy} \Delta t_s}{\Delta y^2} + \frac{D_{zz} \Delta t_s}{\Delta z^2} \leq 0.5$$

$$\Delta t_s \leq \frac{0.5}{\frac{D_{xx}}{\Delta x^2} + \frac{D_{yy}}{\Delta y^2} + \frac{D_{zz}}{\Delta z^2}}$$

Stability criteria (II)

MOC3D

2. Mixing criterion

Change in concentration in element is not allowed to larger than the difference between the present concentration in the element and the concentration in the source

$$\Delta t_s \leq \frac{n_e b_{i,j,k}^k}{Q_{i,j,k}}$$

Files in MOC3D: *_moc.nam and *.obs files

MODFLOW

EXT_MOC_NAM

```

clst  94  ext.out
moc   96  ext.moc
obs   44  ext.obs
data  45  ext.oba
    
```

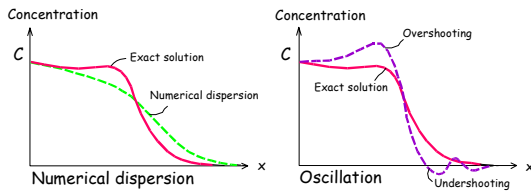
EXT_OBS

```

3 1 ;NUMOBS IOBSFL Observation well data
1 10 10 45 ;layer, row, column, unit number
1 8 10 ;layer, row, column
1 4 10 ;layer, row, column
    
```

NUMERICAL DISPERSION

Numerical dispersion and oscillation



Derivation of numerical dispersion: 1D (I)

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2} - V \frac{\partial C}{\partial x}$$

Discretisation:
backwards in space
backwards in time

By means of Taylor series development:

$$\frac{C_i^k - C_i^{k-1}}{\Delta t} = D \frac{C_{i+1}^k - 2C_i^k + C_{i-1}^k}{\Delta x^2} - V \frac{C_i^k - C_{i-1}^k}{\Delta x}$$

Derivation of numerical dispersion: 1D (II)

Now Taylor series development with truncation errors!

$$\frac{C_i^k - C_i^{k-1}}{\Delta t} = \frac{\partial C}{\partial t} - \frac{\Delta t}{2} \frac{\partial^2 C}{\partial t^2} + \frac{\Delta t^2}{6} \frac{\partial^3 C}{\partial t^3} + O(\Delta t^3)$$

$$\frac{C_i^k - C_{i-1}^k}{\Delta x} = \frac{\partial C}{\partial x} - \frac{\Delta x}{2} \frac{\partial^2 C}{\partial x^2} + \frac{\Delta x^2}{6} \frac{\partial^3 C}{\partial x^3} + O(\Delta x^3)$$

$$\frac{C_{i+1}^k - 2C_i^k + C_{i-1}^k}{\Delta x^2} = \frac{\partial^2 C}{\partial x^2} + \frac{\Delta x^2}{12} \frac{\partial^4 C}{\partial x^4} + O(\Delta x^4)$$

Derivation of numerical dispersion: 1D (III)

$$\frac{C_i^k - C_i^{k-1}}{\Delta t} = D \frac{C_{i+1}^k - 2C_i^k + C_{i-1}^k}{\Delta x^2} - V \frac{C_i^k - C_{i-1}^k}{\Delta x}$$

$$\frac{\partial C}{\partial t} - \frac{\Delta t}{2} \frac{\partial^2 C}{\partial t^2} = D \left(\frac{\partial^2 C}{\partial x^2} + \frac{\Delta x^2}{12} \frac{\partial^4 C}{\partial x^4} \right) - V \left(\frac{\partial C}{\partial x} - \frac{\Delta x}{2} \frac{\partial^2 C}{\partial x^2} + \frac{\Delta x^2}{6} \frac{\partial^3 C}{\partial x^3} \right)$$

Neglect 3rd and 4th order terms:

$$\frac{\partial C}{\partial t} - \frac{\Delta t}{2} \frac{\partial^2 C}{\partial t^2} = D \left(\frac{\partial^2 C}{\partial x^2} \right) - V \left(\frac{\partial C}{\partial x} - \frac{\Delta x}{2} \frac{\partial^2 C}{\partial x^2} \right)$$

Derivation of numerical dispersion: 1D (IV)

$$\begin{aligned} \text{Rewriting term: } & \frac{\partial^2 C}{\partial t^2} \\ \frac{\partial^2 C}{\partial t^2} &= \frac{\partial}{\partial t} \left(\frac{\partial C}{\partial t} \right) = \frac{\partial}{\partial t} \left(D \frac{\partial^2 C}{\partial x^2} - V \frac{\partial C}{\partial x} \right) = D \frac{\partial^3 C}{\partial x^2 \partial t} - V \frac{\partial}{\partial t} \left(\frac{\partial C}{\partial x} \right) \\ \frac{\partial^2 C}{\partial t^2} &= D \frac{\partial^3 C}{\partial x^2 \partial t} - V \frac{\partial}{\partial t} \left(D \frac{\partial^2 C}{\partial x^2} - V \frac{\partial C}{\partial x} \right) \\ \frac{\partial^2 C}{\partial t^2} &= D^2 \frac{\partial^4 C}{\partial x^4} - VD \frac{\partial^3 C}{\partial x^3} - VD \frac{\partial^3 C}{\partial x^3} + V^2 \frac{\partial^2 C}{\partial x^2} \\ \frac{\partial^2 C}{\partial t^2} &\approx V^2 \frac{\partial^2 C}{\partial x^2} \end{aligned}$$

Derivation of numerical dispersion: 1D (V)

Rewrite all extra terms:

$$\begin{aligned} \frac{\partial C}{\partial t} - \frac{\Delta t}{2} \frac{\partial^2 C}{\partial t^2} &= D \left(\frac{\partial^2 C}{\partial x^2} \right) - V \left(\frac{\partial C}{\partial x} - \frac{\Delta x}{2} \frac{\partial^2 C}{\partial x^2} \right) \\ \frac{\partial^2 C}{\partial t^2} &\approx V^2 \frac{\partial^2 C}{\partial x^2} \\ \frac{\partial C}{\partial t} - \frac{\Delta t}{2} V^2 \frac{\partial^2 C}{\partial x^2} &= D \frac{\partial^2 C}{\partial x^2} - V \frac{\partial C}{\partial x} + V \frac{\Delta x}{2} \frac{\partial^2 C}{\partial x^2} \\ \frac{\partial C}{\partial t} &= \left(D + V \frac{\Delta x}{2} + \frac{\Delta t}{2} V^2 \right) \frac{\partial^2 C}{\partial x^2} - V \frac{\partial C}{\partial x} \end{aligned}$$

IMPORTANT

Derivation of numerical dispersion: 1D (VI)

Numerical dispersion:

$$D = D_{real} + V \frac{\Delta x}{2} + \frac{\Delta t}{2} V^2$$

Remedy to reduce numerical dispersion:

1. Δx en Δt smaller
2. Use a different numeric scheme (Crank-Nicolson)
3. Use a smaller D_{real}

EVERYTHING YOU ALWAYS WANTED TO KNOW

Modelling for Chemists

1. *Everything you always wanted to know about modelling, and now you know it?*
2. *Everything you always wanted to know about modelling, and now you are definitely afraid to ask?*

Additional information:

Groundwater modelling: <ftp://ftp.geo.uu.nl/pub/people/geo/gwm1/gwm1.pdf>

Density dependent groundwater flow: <ftp://ftp.geo.uu.nl/pub/people/geo/gwm2/gwm2.pdf>

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